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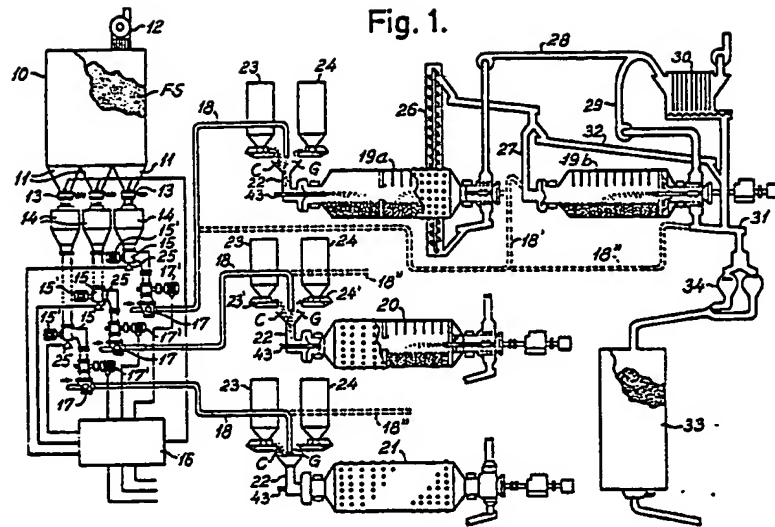
(54) A method and a plant for producing a dry cement composition.

(57) The invention relates to a method of producing a dry cement composition, said method comprising feeding a continuous flow of a starting material (C, G), which includes cement binder clinker (C) and a content of water soluble chromate, to a cement mill (19 - 21), grinding the starting material in the cement mill while introducing a cooling medium into the mill so as to maintain the temperature of the material in the mill at a desired level, continuously discharging the ground cement material from the cement mill, and transferring the ground cement material to a storage container (33), characterized in that ferrous sulfate ( $\text{FeSO}_4 \cdot n\text{H}_2\text{O}$ ) in an amount of 0.01 - 10 percent by weight is added to and mixed with said flow of material in a dry or non-dissolved condition at a location or at locations upstream of said storage container (33) in order to eliminate or substantially reduce said content of water-soluble chromate. Furthermore, the invention relates to a plant for carrying out the aforementioned method.

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Fig. 1.



# A METHOD AND A PLANT FOR PRODUCING A DRY CEMENT COMPOSITION.

The present invention relates to a method and a plant for producing a dry cement composition which, when mixed with water, gives an immeasurable or low concentration of  $\text{Cr}^{+6}$  (in the following also called "chromate") dissolved in the water.

Cement is normally manufactured by grinding a starting material including cement binder clinker and gypsum, and in some cases also other additives, such as fly ash, slag, puzzolane, and grinding aid, the starting material being continuously supplied to and ground in a cement mill. The conventional cement mill is a ball grinder comprising a rotating drum with very large dimensions, such as a length of 15 m and a diameter of 5 m. In operation such a huge ball grinder generates an excessive amount of heat. In order to prevent the temperature in the mill from exceeding an acceptable level, the mill is normally cooled by spraying or atomizing water into the inner space of the rotating drum. Consequently, the atmosphere within a conventional cement mill has a relatively high temperature (normally 120 - 140°C) and a high humidity (about 0.3 kg water vapour per kg air). Thus, the cement material is exposed to rather vigorous conditions when treated in the cement mill. Furthermore, during the manufacturing process ground cement composition is normally transported by means of pneumatic transporting devices whereby almost each single cement particle is brought into intimate contact with the transporting air.

It has been known for a long time that cements contain chromium compounds which, when cements are mixed with water, appear as  $\text{Cr}^{+6}$  dissolved in the water, and that this dissolved chromate is objectionable from a health point of view, because it may cause eczema in persons working with the cement-water mixtures when it comes into contact with their skin.

It is known to reduce the concentration of dissolved chromate in a cement-water mixture and in wet concrete by adding ferrous sulfate during the mixing process for producing said mixture. The ferrous

- ion of ferrous sulfate reduces the  $\text{Cr}^{+6}$  to  $\text{Cr}^{+3}$  which is only slightly soluble in cement-water mixtures. In "Annex 3 to circular letter 15" issued by CEMBUREAU (European Cement Association), Paris, and dated 1st March, 1979, it is proposed to dissolve the ferrous sulfate as a 20% solution before the addition. Said annex also describes an experiment in which it was attempted to add the ferrous sulfate solution during the manufacturing process of the cement. The ferrous sulfate was sprayed into the hot and humid clinker in a cement mill together with gypsum. The annex concludes that hardly any chromate was then reduced, even if double the normal dose of ferrous sulfate was added. A better, but still unsatisfactory result was obtained by heating the clinker and gypsum to  $140^{\circ}\text{C}$  after milling and spraying a solution of ferrous sulfate on the hot cement. Furthermore, in a paper issued by CEMENTA AB and dated 13th October, 1977 the authors of the above publication state that ferrous sulfate cannot be added prior to grinding in a cement factory because the environment in the mill causes iron(II) sulfate to oxidize into inactive iron(III) sulfate, and it is concluded that no practical possibility of eliminating chromium compounds in the cement manufacture exists.
- U.S. Patent Specification No. 3,425,892 issued on 4th February, 1969, discloses a cement composition containing 0.1 - 5% of ferrous sulfate for the purpose of retarding the hardening rate of the cement composition. Said U.S. patent does not at all relate to reduction of water-soluble chromate in cement mixtures.
- It has now been found that contrary to the teachings of the above mentioned publications from CEMBUREAU and CEMENTA it is possible to reduce the content of dissolved chromate in a cement-water mixture and in wet concrete by adding ferrous sulfate to the cement during the manufacturing stage, namely if the ferrous sulfate is added in a dry or non-dissolved condition.

Thus, the present invention provides a method of producing a dry cement composition, said method comprising feeding a continuous flow of a starting material, which includes cement binder clinker and a content of water-soluble chromate, to a cement mill, grinding the

starting material in the cement mill while introducing a cooling medium, such as air or water, into the mill so as to maintain the temperature of the material in the mill at a desired level, continuously discharging the ground cement material from the cement mill, and  
5 transferring ground cement material to a storage container, and the method according to the invention is characterized in that ferrous sulfate ( $\text{FeSO}_4 \cdot n\text{H}_2\text{O}$ ) in an amount of 0.1 - 10% by weight is added to and mixed with said flow of material\* at a location or at locations upstream of said storage container in order to eliminate or substantially  
10 reduce said content of water-soluble chromate.

Surprisingly, it has been found that ferrous sulfate is able to resist the rather extreme temperature and humidity conditions existing within the cement mill without an unacceptable reduction of its chromate-reducing ability, provided that the ferrous sulfate is added in a  
15 dry or non-dissolved condition.

The amount of ferrous sulfate to be added depends i.a. on the amount of chromate contained in the cement, and as the chromate-reducing ability of the ferrous sulfate may decrease during the period of time in which the finished cement composition is stored before use, the  
20 necessary amount of ferrous sulfate may also depend on the stipulated storage time of the cement composition. The longer the cement mixture is to be stored, the more ferrous sulfate is required.

In the present context, the terms "cement", "cement composition", and "cement mixture" comprises Portland cement types, including  
25 ordinary cement, rapid-hardening cement and super-rapid-hardening cement, high alumina cement, belite cement, and low heat cement; and blended cements puzzolan cements, slag cements, etc., in particular Portland cements and blended cements.

It is believed that the tendency of decrease in the chromate-reducing  
30 ability of the ferrous sulfate may be avoided or to some extent diminished if the ferrous sulfate is in the form of a particulate material in which the particles are provided with an oxidation-preventing coating.

\* in a dry or non-dissolved condition and

Ferrous sulfate of this type is marketed by Melchemie B.V., Arnhem, Holland, under the trade marks MELSTAR and FERROMEL-20. In the method of the present invention, it may be advantageous to use ferrous sulfate with particles which are provided with a coating which is even thicker than that used in the product sold under the above trade marks.

The ferrous sulfate may be added in an amount of 0.01 - 5, preferably 0.1 - 1 percent by weight. If the amount exceeds 1 percent, the ferrous sulfate may have an undesired retarding effect on the hardening rate of the cement mixture when water and aggregate have been added thereto. A still more preferred amount of ferrous sulfate is 0.3 - 1 percent. At present an amount of about 0.4 percent by weight is especially preferred in connection with cement compositions of the type in which the starting material comprises clinker made from clay and chalk, while a smaller percentage of ferrous sulfate, such as 0.1 percent, may be sufficient when the clinkers are made from sand and chalk, because the contents of chromium compositions in sand are substantially smaller than in clay.

The ferrous sulfate may be added to the flow of starting material at one or more suitable locations upstream of the storage container. Thus, the total metered flow of the ferrous sulfate or at least part thereof is preferably added to the starting material upstream of the cement mill in which ferrous sulfate is very thoroughly mixed with the starting material during the grinding process taking place therein. As explained above, rude conditions within the cement mill may to some extent reduce the chromate-reducing ability of the ferrous sulfate. Therefore, when the cement mill is of a multistage type, the ferrous sulfate or at least part thereof is preferably added to the starting material between consecutive stages of the mill, and advantageously between the last stage but one and the last stage. Thereby the desired thorough mixing of the starting material and the ferrous sulfate is obtained, while the residence time of the ferrous sulfate within the mill is reduced to a minimum.

It is also possible to add the ferrous sulfate or at least part thereof to the ground starting material at a location downstream of the cement mill and upstream of the storage container, for example at the inlet of a pneumatic transporting device for transporting the ground cement material to the storage container. The ground cement material and the particulate ferrous sulfate added thereto downstream of the cement mill may be sufficiently intermixed by passing the pneumatic transporting device. However, it is also possible to increase the mixing efficiency by passing the flow of material through a special mixing device of any suitable type. Provided that it is possible to obtain an efficient mixing of the components of the cement composition, the amount of ferrous sulfate added to the starting material downstream of the cement mill may be somewhat smaller than when the sulfate is added upstream of the cement mill.

The content of ferrous sulfate in the finished cement composition retards the hardening rate of concrete made from this cement composition. It has been found, however, that this side effect is without any significance, especially when the amount of ferrous sulfate added is less than one percent, which is normally the case. The content of ferrous sulfate in the cement composition also causes a "thickening effect" which means that poured and vibrated concrete made from the cement composition does not tend to separate water on the surface like concrete made from a cement composition without ferrous sulfate.

The invention also relates to a plant for carrying out the method described above which comprises at least one cement mill, feeding means for feeding a continuous flow of a starting material, including cement binder clinker, to the mill, a storage container for the finished cement composition, and transporting means for transporting ground cement material discharged from the mill to the storage container, and the plant according to the invention is characterized in that it further comprises a supply container for ferrous sulfate and metering means for feeding a metered continuous flow of ferrous sulfate from the supply container into the flow of starting material at a location or at locations upstream of the storage container.

The invention will now be further described with reference to the drawings, wherein

Fig. 1 diagrammatically illustrates a cement producing plant according to the invention, in which ferrous sulfate is fed from a common silo to  
5 cement mills connected in parallel to the silo, and

Fig. 2 diagrammatically illustrates part of a modified embodiment of the plant shown in Fig. 1.

The cement producing plant illustrated in Fig. 1 comprises a silo 10 having three funnel outlets 11 at the bottom and a filter 12 at the top. The silo contains particulate ferrous sulfate FS of the previously mentioned type sold under the trade marks MELSTAR and FERRO-MEL-20. Suitable batches of ferrous sulfate may be removed from the outlets 11 by means of selectively operatable vibrating devices 13 and collected in corresponding containers 14. Metering devices 15 are  
15 positioned at the bottoms of the containers 14 and each of the metering devices may comprise a screw conveyor driven by an electric motor 15', which may be controlled by an electronic control device 16 as described in further detail below. Each of the metering devices 15 provides a continuous, controlled, metered flow of ferrous sulfate  
20 through an air sluice 17' and into a pneumatic transporting device 17 comprising a transporting conduit 18. The conduits 18 are connected to three different mills 19a, 20, and 21 in three otherwise separated cement producing plants. A starting material comprising cement binder clinker C, gypsum G and possible other components, is supplied to  
25 the inlet 22 of each mill. In the drawings two feeding devices 23 and 24 provided with corresponding measuring devices, 23' og 24', respectively, for feeding a continuous flow of cement binder clinker and gypsum, respectively, are illustrated, and the transporting conduits 18 open into the inlet 22 so that the metered flow of ferrous sulfate  
30 provided by each of the metering devices 15 is added to the starting material at the cement mill inlet 22.

Each of the containers 14 and the associated metering device 15 forms a unit which is supported by a weighing cell 25. This cell generates weight signals representing the actual total weight of the associated  
35 unit. It is understood that the rate of weight reduction of each unit corresponds to the rate at which ferrous sulfate is fed to the trans-



porting device 17 by means of the corresponding metering device 15. Therefore, the control device 16 may control the feeding rates of the metering devices 15 in response to signals received from the weighing cells 25 and to corresponding signals received from feeding devices  
5 for feeding starting material to the cement mills, so as to secure that a desired percentage by weight of ferrous sulfate is continuously added to the starting material fed to each of the cement mills 19a, 20 and 21. When the amount of ferrous sulfate contained in one or more of the containers 14 has reached a predetermined minimum, which  
10 means that the corresponding weighing cell 25 has determined a predetermined minimum weight of the corresponding unit, the control device 16 may establish communication between the silo 10 and the container 14 and operate the corresponding vibrating device 13 so as to fill a new batch of ferrous sulfate from the silo 10 into the corres-  
15 ponding container 14.

Apart from the system described above for feeding metered flows of ferrous sulfate to the respective cement mills, the cement production plants shown in the drawings are of known types. In the upper part of Fig. 1 a two stage grinding plant comprising two separate mills 19a  
20 and 19b, which are connected in series, is shown. As mentioned above, the ferrous sulfate may be supplied to the inlet 22 of the cement mill 19a through the conduit 18. However, the supply of ferrous sulfate may, alternatively or additionally, be supplied to the inlet of the last mill 19b through a transport conduit 18' and/or to  
25 outlets of the mill b through a transport conduit 18" as indicated with broken lines in Fig. 1.

The ground cement material leaving the cement mill 19a is lifted by an elevator 26 and passed to the inlet of the cement mill 19b through a conduit 27. Ventilating air from the cement mills 19a and 19b is con-  
30 veyed through conduits 28 and 29 to an electrostatic precipitator 30 and exhausted into the atmosphere. Dust material separated from the air by the precipitator 30 is delivered to an outlet transporting device 31 which is also connected to the outlet of the cement mill 19b. The finished cement composition from the outlet transporting device 31 may  
35 be conveyed to a storage silo 33 by means of a suitable mechanical or

pneumatic transporting device 34. Ground cement composition from the mill 19a may by-pass the mill 19b through a transporting device 32 if it is desired to operate the plant with one mill only.

In case the ferrous sulfate is supplied to the plant at two or more locations, different types of chromate reducing agents may be added at the various locations. For example, ferrous sulfate could be added at the inlet 22, and other suitable chemical compositions could be added between the mills 19a and 19b or between the mill 19b and the storage silo 33. Alternatively, ferrous sulfate in particulate form with coated particles as described above could be added at the inlet 22, and dried particulate ferrous sulfate with uncoated particles could be supplied at one or both of the other locations, or vice versa.

Fig. 2 shows a cement grinding plant with a single cement mill 20, and parts corresponding to those shown in Fig. 1 have been designated with the same reference numerals. The ground material leaving the outlet of the cement mill is lifted by the elevator 26 and delivered to an air separator 44 through a transporting device 35. The separator separates finer particles from coarser particles. The coarser particles are returned to the inlet of the cement mill 20 through a return transporting device 36, while air or gas and the finer particles are passed to a cyclone 37. In the cyclone 37 the solid material is separated from the air which is recycled through a transporting device 38, while the finer particles of the solid material is passed to a product outlet 39 through a transporting device 40. The finished product is transported from the product outlet 39 to a suitable storage site, such as a silo 33 by means of a pneumatic transporting device 34.

In operation, the mills 19 - 21 are rotated together with cement material and grinding balls contained therein. The mechanical energy thus supplied to the mills is converted into heat energy. In order to maintain the temperature in the mills at an acceptable level, normally within the temperature range 120 - 140°C, a cooling liquid, normally cooling water, is sprayed or atomized within the mills by means of suitable spraying devices 43. Consequently, the atmosphere within the cement mills is very humid.

In a plant of the type shown in Fig. 2 the ferrous sulfate may be supplied through the conduit 18 to the conduit 36 returning coarse material from the separator 44. However, the ferrous sulfate may, alternatively or additionally, be supplied to the transporting device 40 through a conduit 41 and/or to the outlet of the mill 20 through a conduit 42 indicated with broken lines.

It should be understood that any of the cement mills 20 and 21 shown in Fig. 1 may constitute part of a grinding plant like any of those shown in the upper part of Fig. 1 or in Fig. 2, or of any other known type. Furthermore, the ferrous sulfate may be supplied to the grinding plant in dry condition at any suitable location securing a thorough mixing with the other cement components.

#### EXAMPLE 1.

In a cement-producing plant of the type illustrated in Fig. 2, rapid hardening cement was ground in a cement mill, and a chromate-reducing agent comprising 96%  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  and provided with an oxidation-preventing coating ("MELSTAR") was metered to the inlet 22 of the mill 20. The final cement product was transported about 350 m by means of the pneumatic transporting device 34 from the cement mill 20 to the storage silo 33.

The amount of ferrous sulfate added was 0.47%, calculated on the weight of the cement. At the start of the experiment, the cement contained 8.2 ppm Cr water-soluble chromate which is a typical value. Samples were withdrawn every hour immediately after the product had left the cement mill.

During the sampling for 7 hours after the start of the experiment, practically no water-soluble chromate could be detected in the cement samples. The dosage of ferrous sulfate was then reduced to 0.40%. During the last three hours of the experiment, a small, but measurable content of water-soluble chromate in the cement was detected in the samples taken immediately after the product had left the mill. In

comparison with laboratory experiments, it was found that the same satisfactory extent of reduction of water-soluble chromate required 0.47% of ferrous sulfate, calculated on the cement, in the production plant, compared with 0.35% in the laboratory experiment.

- 5 A sample taken from the silo 33 immediately after the termination of the experiment showed a low value of water-soluble chromate which was of the same order as the value for the last three hours of production. This indicates that the reducing capacity of the 0.4% of ferrous sulfate in the cement which had been transported about 350 m  
10 by a pneumatic conveyor was not deteriorated by the major exposure to air during transport.

The amount of water-soluble chromate in the cement was determined by extracting a cement sample (3 g) with a 20% solution of sodium sulfate and measuring the amount of dissolved chromate in the extract  
15 by a colorimetric diphenyl carbazide method using a 5 cm cuvette in the spectrophotometer to ensure maximum sensitivity. The results of the above experiments appear from table I below:

TABLE I

<i>Sampling time</i>		<i>Free chromate ppm Cr.</i>
<i>Date</i>	<i>Hour</i>	
20	28.02.80 11.00	8.2
	28.02.80 12.00	<0.1
	28.02.80 14.30	<0.1
	28.02.80 15.00	<0.1
25	28.02.80 16.00	<0.1
	28.02.80 18.00	<0.1
	28.02.80 19.00	<0.1
	28.02.80 20.00	<0.1
	28.02.80 21.00	0.5
30	28.02.80 22.00	0.2
	28.02.80 23.00	0.1

(Table continued):

Average	0.3
Silo (Sample taken from the silo after termination of the run)	0.1

5 Within a period of 3 months after storing the cement mixture in the  
storage silo, samples were taken from the bottom of the silo in connec-  
tion with delivery of cement from the silo, and the contents of water-  
soluble chromate in the samples were determined. The content of  
10 water-soluble chromate in the cement as a function of storage time in  
the silo appears from table II. During the first 11 days the content of  
water-soluble chromate increases to 1 ppm Cr, and during the follow-  
ing two months, the content of water-soluble chromate varies between  
1 and 2 ppm Cr. This indicates that there is a minor decrease in the  
15 reducing capacity of the ferrous sulfate, but the ferrous sulfate is  
still capable of reducing 75 - 90% of the original content of water-  
soluble chromate in the cement even after 2 - 3 months of storage.

It should be noted that the theoretical amount of ferrous sulfate  
which would stoichiometrically correspond to reduction of the initial  
concentration of water-soluble chromate in the cement is only 0.013%  
20  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ , in other words, the amount of ferrous sulfate added in  
the above experiment represents an excess of more than 30 times,  
which is presumed to be due to other chemical reactions taking place.  
It is envisaged that the use of ferrous sulfate containing a more  
efficient coating and/or the addition of ferrous sulfate at different  
25 stages during the production may reduce the amount of ferrous sul-  
fate necessary for obtaining an adequate chromate-reducing effect.

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TABLE II

<i>Date</i>	<i>Storage time, days</i>	<i>Water-soluble chromate ppm Cr</i>
5 29.02.80	0	0.3
10.03.80	11	1.0
27.03.80	28	1.0
16.04.80	48	1.0
20.05.80	82	0.9 - 2.1

## 10 EXAMPLE 2

An experiment similar to that described in example 1 was carried out in a cement-producing plant of the same type. The amount of ferrous sulfate ( $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ ) added was 0.6% calculated on the weight of the cement. At the start of the experiment, the cement contained 10.0 ppm Cr water-soluble chromate. A sample was withdrawn every hour immediately after the product had left the cement mill, and the samples for each period of eight hours were mixed to constitute a representative sample for the respective period. The amount of water-soluble chromate in the cement was determined as described in example 1. The results obtained are stated in table III:

TABLE III

<i>Sampling time</i>		<i>Free chromate ppm Cr</i>
<i>Date</i>	<i>Hour</i>	
07.10.80	14 - 22	<0.1
5 07.10.80	22 - 06	<0.1
08.10.80	06 - 14	<0.1
08.10.80	14 - 22	<0.1
08.10.80	22 - 06	<0.1
09.10.80	06 - 14	0.1
10 09.10.80	14 - 22	<0.1
09.10.80	22 - 06	<0.1
10.10.80	06 - 14	<0.1
10.10.80	14 - 22	<0.1

15 It appears that in almost all of the samples the content of water-soluble chromate was less than 0.1 ppm Cr, i.e. the amount was below the measuring limit. Within a period of 63 days after storing the cement composition in the storage silo, batches were removed and delivered to a selected customer, and simultaneously, a sample was taken from each batch. The content of water-soluble chromate was  
20 determined for each of the samples of cement in the manner described above, and also for a sample of each of the batches after mixing them with water in a concrete mixer. The results obtained are stated below in table IV:

TABLE IV

	<i>Date</i>	<i>Storage time, days</i>	<i>Water-soluble chromate ppm Cr</i>	
			<i>Samples from cement</i>	<i>Samples from wet concrete</i>
5	08.10.80	0	<0.1	<0.1
	27.10.80	19	<0.1	<0.1
	28.10.80	20	<0.1	<0.1
	29.10.80	21	<0.1	<0.1
	30.10.80	22	<0.1	<0.1
10	31.10.80	23	<0.1	<0.1
	05.11.80	28	<0.1	<0.1
	13.11.80	36	1.5	<0.1
	19.11.80	42	<0.1	<0.1
	26.11.80	49	<0.1	<0.1
15	03.12.80	56	0.4	<0.1
	10.12.80	63	0.4	<0.1

It appears that no content of water-soluble chromate could be determined in the batches of wet concrete mixture, while smaller amounts were determined in three of the cement samples taken.

- 20 This is probably due to the fact that the samples taken out are less representative and more influenced by incidental variations than the batches which were thoroughly mixed in a concrete mixer before determination of the chromate content.

### EXAMPLE 3

- 25 In a cement-producing plant corresponding to that shown in Fig. 1 ferrous sulfate was supplied to three different cement-grinding plants connected in parallel, from a common silo in the manner illustrated in Fig. 1. Two of the cement-grinding plants each included two cement mills connected in series, and the third grinding plant contained a
- 30 single cement mill.



The ferrous sulfate, which was of the type marketed by Melchemie B.V., Arnhem, Holland, under the trade mark FERROMEL-20, was added in an amount of 0.4 per cent by weight. In the two-stage grinding plants, ferrous sulfate was added between the mills, while  
5 the ferrous sulfate was added at the inlet of the mill in the single-stage plant.

During a period of 2 1/2 months, four different types of cement were produced, namely normal Portland cement, rapid-hardening cement, low alkali/sulfate-resistant cement, and Portland cement containing fly  
10 ash. Every day in the said 2 1/2 months period, a representative sample of the production of the day was taken at the outlet of each of the grinding plants.

The amount of water-soluble chromate in the cement was determined by extracting each cement sample (3 g) with pure water, and  
15 measuring the amount of dissolved chromate in the extract by a colorimetric diphenyl carbazide method using a 5 cm cuvette in the spectrophotometer to ensure maximum sensitivity. No measurable content of water-soluble chromate was detected in any of the samples, which means that the content of free chromate was less than 0.1 ppm  
20 Cr.

## CLAIMS

1. A method of producing a dry cement composition, said method comprising feeding a continuous flow of a starting material (C, G), which includes cement binder clinker (C) and a content of water soluble chromate, to a cement mill (19 - 21), grinding the starting material in the cement mill while introducing a cooling medium into the mill so as to maintain the temperature of the material in the mill at a desired level, continuously discharging the ground cement material from the cement mill, and transferring the ground cement material to a storage container (33),
- 5 characterized in that ferrous sulfate ( $\text{FeSO}_4 \cdot n\text{H}_2\text{O}$ ) in an amount of 0.01 - 10 percent by weight is added to and mixed with said flow of material \*at a location or at locations upstream of said storage container (33) in order to eliminate or substantially reduce said content
- 10 of water-soluble chromate.
2. A method according to claim 1, characterized in that the ferrous sulfate is a particulate material the particles of which are provided with an oxidation preventing coating.
3. A method according to claim 1 or 2,
- 20 characterized in that the ferrous sulfate is added in an amount of 0.01 - 5 and preferably 0.1 - 1 percent by weight.
4. A method according to claim 3, characterized in that the ferrous sulfate is added in an amount of 0.3 - 1 and preferably of about 0.4 or 0.6 percent by weight.
- 25 5. A method according to any of the claims 1 - 4, characterized in that a metered flow of ferrous sulfate is added to the starting material upstream of the cement mill.
6. A method according to any of the claims 1 - 4, wherein the cement mill (19) is of a multistage type,
- 30 characterized in that the ferrous sulfate is added to the starting material between consecutive stages (19a, 19b) of the mill.
- \* in a dry or non-dissolved condition

7. A method according to any of the claims 1 - 4,  
characterized in that the ferrous sulfate is added to and mixed with  
the ground starting material at a location downstream of the cement  
mill and upstream of the storage container.
- 5 8. A plant for carrying out the method according to any of the claims  
1 - 7 which comprises at least one cement mill (19 - 21), feeding  
means (23, 24) for feeding a continuous flow of a starting material  
(C, G), including cement binder clinker (C), to the mill, a storage  
10 container (33) for finished cement composition, and transporting  
means (31) for transporting ground cement material discharged from  
the mill to the storage container (33),  
characterized in that the plant further comprises a supply container  
(14) for ferrous sulfate (FS), and metering means (15) for feeding a  
15 metered continuous flow of ferrous sulfate from the supply container  
into the flow of starting material at a location or at locations upstream  
of the storage container.
9. A plant according to claim 8,  
characterized in that the metering means (15) are adapted to feed  
ferrous sulfate (FS) into the flow of starting material at a location  
20 upstream of the cement mill (19 - 21).
10. A plant according to claim 8 or 9 and comprising a pair of cement  
mills (19a, 19b) connected in series,  
characterized in that the metering means (15) are adapted to feed  
ferrous sulfate into the flow of ground material at a location (18')  
25 between the cement mills.
11. A plant according to any of the claims 8 - 10,  
characterized in that the metering means are adapted to feed ferrous  
sulfate into the flow of ground cement material at the transporting  
means (31).
- 30 12. A plant according to any of the claims 8 - 11,  
characterized in first measuring means (23' 24') for measuring the  
mass flow of the starting material (C, G) supplied to the cement mill

(19, 21) by the feeding means, second measuring means (25) for determining the mass flow of the ferrous sulfate (FS) fed by the metering means (15) to the flow of starting material, and control means (16) for controlling the feeding rate of the metering means (15) in relation to the feeding rate of the feeding means (23', 24'), in response to measuring signals received from said first and second measuring means.

13. A dry cement composition produced by the method according to any of the claims 1 - 7.

10 14. A dry cement composition packed for shipment to the final user, characterized in containing ferrous sulfate in an amount of 0.01 - 10 percent by weight, which has been added in a dry condition at the production of the cement composition.

15 15. A cement composition according to claim 14, characterized in that the ferrous sulfate is a particulate material, the particles of which are provided with an oxidation preventing coating.

16. A cement composition according to claim 14 or 15, characterized in that ferrous sulfate has been added in an amount of 0.1 - 1 percent by weight.

20 17. A cement composition according to claim 16, characterized in that ferrous sulfate has been added in an amount of 0.3 - 1, preferably 0.4 - 0.6 percent by weight.

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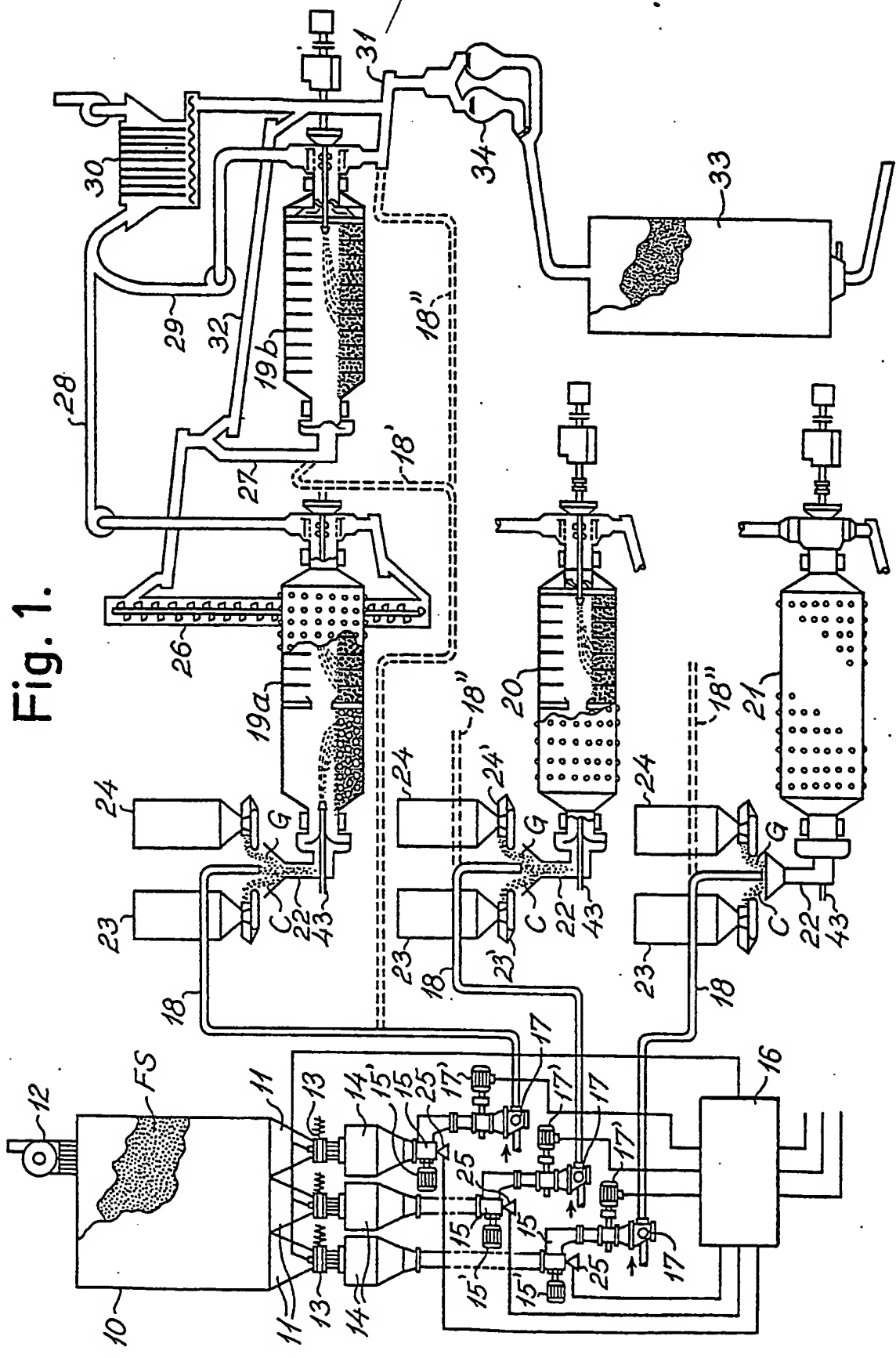
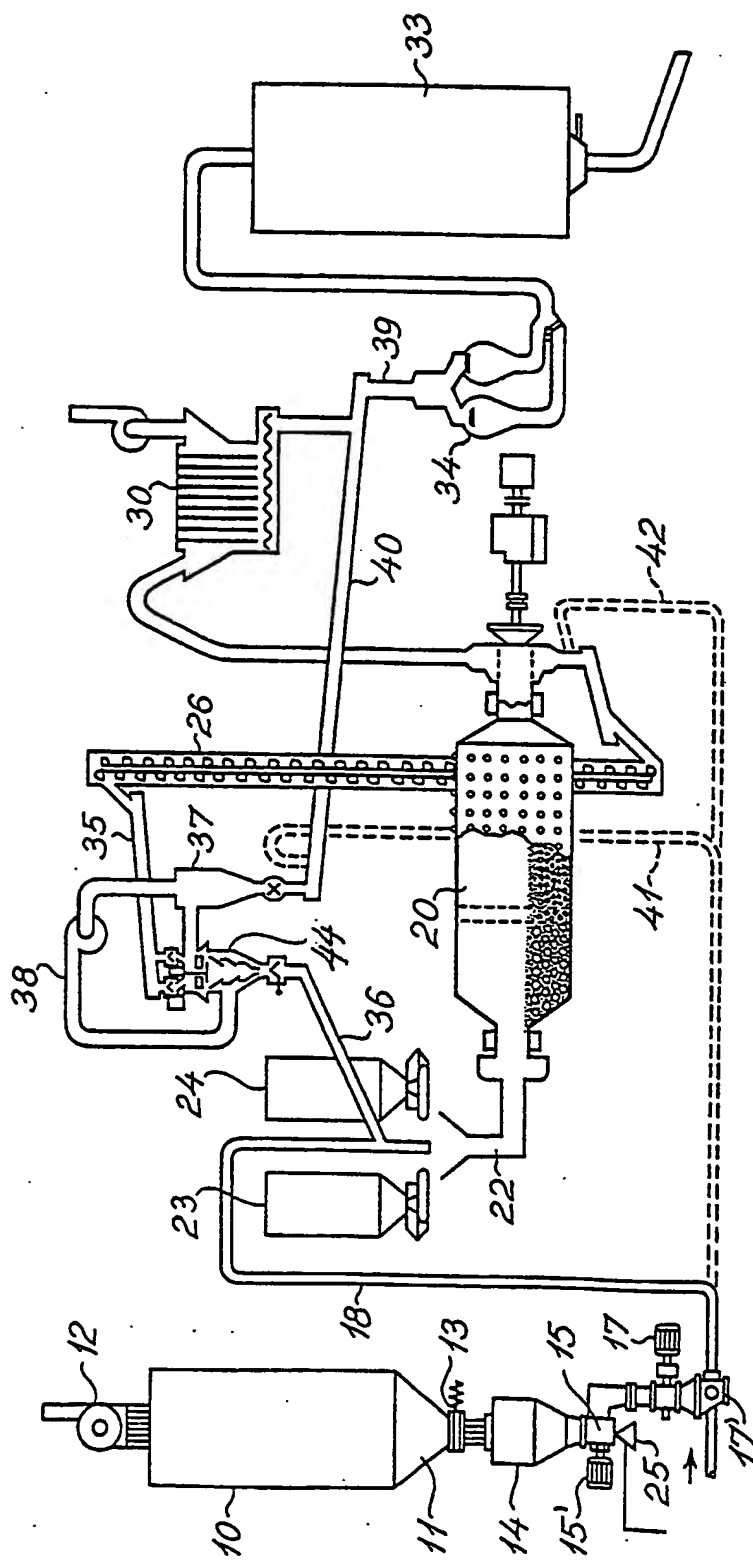


Fig. 1.

Fig. 2.





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0054314

Application number

EP 81 11 0557.6

DOCUMENTS CONSIDERED TO BE RELEVANT			CLASSIFICATION OF THE APPLICATION (Int. Cl. 3)
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	
X	CH - A - 534 643 (SERVICE NEUCHATELOIS DE MEDECINE DU TRAVAIL ET D'HYGIENE INDUSTRIELLE) * claims; tables *	1,3,5, 13	C 04 B 7/35 C 04 B 7/48 //C 04 B 13/22
Y,D	US - A - 3 425 892 (M.R. EDELSON et al.) * claims 1, 3, 4; column 3, lines 1 to 14 *	1,3,5, 7,13	
Y	Chemical Abstracts vol. 79, no. 16 22 October 1973 Columbus, Ohio, USA S. FREGERT et al. "Factors decreasing the content of water-soluble chromate in cement" page 271, column 2, abstract no. 96214c & Acta Derm.-Venereol., vol. 53, no. 4 1973, pages 267 to 270	1,3	TECHNICAL FIELDS SEARCHED (Int. Cl. 3)  C 01 G 37/00 C 01 G 49/14 C 04 B 7/00 C 04 B 13/00 C 04 B 31/00
A	Chemical Abstracts vol. 88, no. 20 15 May 1978 Columbus, Ohio, USA M.H. LUND "Chromium in cement" page 273, column 2 to page 274, column 1, abstract no. 140777a & Nord. Betong, no. 6, 1977, pages 28 to 30 ./..	1,3	CATEGORY OF CITED DOCUMENTS  X: particularly relevant if taken alone Y: particularly relevant if combined with another document of the same category A: technological background O: non-written disclosure P: intermediate document T: theory or principle underlying the invention E: earlier patent document, but published on, or after the filing date D: document cited in the application L: document cited for other reasons
<input checked="" type="checkbox"/> The present search report has been drawn up for all claims			&: member of the same patent family, corresponding document
Place of search Berlin		Date of completion of the search 26-02-1982	Examiner STROUD

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Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	
A	<p>Chemical Abstracts vol. 90, no. 22 28 May 1979 Columbus, Ohio, USA S. FREGERT et al. "Reduction of chromate in cement by iron sulfate" page 339, column 2, abstract no. 173877c &amp; Contact Dermatitis, vol. 5, no. 1, 1979, pages 39 to 42</p>	1,3,4	
A	<p><u>US - A - 2 316 039</u> (H.R. WILSON)</p>		<p>TECHNICAL FIELDS SEARCHED (Int. Cl.)</p>



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